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# Use of a Novel Extremophilic Xylanase for an Environmentally Friendly Industrial Bleaching of Kraft Pulps

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**Abstract:** Xylanases can boost pulp bleachability in Elemental Chlorine Free (ECF) processes, but their industrial implementation for producing bleached kraft pulps is not straightforward. It requires enzymes to be active and stable at the extreme conditions of alkalinity and high temperature typical of this industrial process; most commercial enzymes are unable to withstand these conditions. In this work, a novel highly thermo and alkaline-tolerant xylanase from *Pseudothermotoga thermarum* was overproduced in *E. coli* and tested as a bleaching booster of hardwood kraft pulps to save chlorine dioxide (ClO<sub>2</sub>) during ECF bleaching. The extremozyme-stage (EXZ) was carried out at 90 °C and pH 10.5 and optimised at lab scale on an industrial oxygen-delignified eucalyptus pulp, enabling us to save 15% ClO<sub>2</sub> to reach the mill brightness, and with no detrimental effect on paper properties. Then, the EXZ-assisted bleaching sequence was validated at pilot scale under industrial conditions, achieving 25% ClO<sub>2</sub> savings and reducing the generation of organochlorinated compounds (AOX) by 18%, while maintaining pulp quality and papermaking properties. Technology reproducibility was confirmed with another industrial kraft pulp from a mix of hardwoods. The new enzymatic technology constitutes a realistic step towards environmentally friendly production of kraft pulps through industrial integration of biotechnology.

**Keywords:** extremophilic xylanase; kraft pulp; ECF bleaching; chlorine dioxide savings

## 1. Introduction

Global concern about climate change has led authorities and governments to implement strategies and rules to address the protection of the environment and natural habitats. In line with the 2030 Agenda for Sustainable Development, the European Green Deal encompasses a set of measures for sustainable growth towards a circular economy, such as more restrictive laws against polluting processes and the investment in environmentally friendly technologies to force industries to make a transition towards cleaner and greener processes. Even before this, the pulp and paper industry had already undergone a major transformation towards the development of cleaner processes in the past few decades, particularly in the pulp bleaching plant. The concern about formation of chlorinated dioxins and other chlorinated compounds during pulp bleaching resulted in a technological revolution in the pulp industry. However, the commitment to remove elemental chlorine (responsible for the formation of chlorinated dioxins) from pulp production in ECF pulps, and thereafter to eliminate chlorine-derived reagents (i.e., chlorine

dioxide) in the so-called totally chlorine free (TCF) processes, requires the development and optimisation of new bleaching sequences [1–4]. In this endeavour, biotechnology can significantly help with the transition to greener pulp production industrial processes. The use of different types of enzymes as biocatalysts to aid pulp bleaching and delignification has been widely reported [5–7]. Laccases and xylanases are the preferred biocatalysts used as “prebleaching” or “bleaching boosters” to improve pulp bleachability. For instance, xylanase treatment of pulp after oxygen delignification has been shown to be effective in some ECF sequences [5–8], allowing fewer bleaching chemicals to be used, which has economic benefits.

During kraft pulping, short xylan chains precipitate at the surface of the fibres acting as a physical barrier against the action of the bleaching agents [9], leading to substantial consumption of  $\text{ClO}_2$ . Pretreatment of pulp with xylanases boosts the action of the bleaching chemicals by breaking the xylans and subsequently reducing the concentration of long xylan chains on the fibre surface, which increases their permeability [10]. Nevertheless, for the feasible integration of an enzymatic stage in the industrial process, the enzyme must be active and stable at the operating industrial conditions. This is particularly relevant for the kraft process, given the harsh physicochemical conditions that characterise this pulping method, which is used predominantly by the paper industry to obtain pulp from wood. Most of the commercial enzymes are unable to withstand the conditions of high temperatures and alkaline pH used in this particular industry [11].

The great diversity of microorganisms capable of colonising diverse habitats in nature constitutes many potential sources of enzymes for industry. In particular, extremophilic bacteria or archaea adapted to extreme temperatures, pH, pressure or salinity become valuable sources of enzymes to be applied as biocatalysts at the harsh operational conditions of the industrial processes [12]. In silico screening of protein sequences from databases, often derived from genomic and metagenomic analysis, has been successfully applied to identify extremophilic enzymes [11,13,14].

A bioinformatic screening of the glycosyl hydrolase family GH10 allowed the identification and characterisation of xylanases active at high pH and temperature. One enzyme in particular, Xyn11, a xylanase from *Pseudothermotoga thermarum*, showed an exceptional xylanolytic activity at 90 °C and pH 10.5 [11]. Here, this extremophilic enzyme (extremozyme) is integrated in an industrial ECF bleaching sequence of eucalyptus kraft pulp with the aim of increasing pulp bleachability and reducing the need for  $\text{ClO}_2$  as bleaching agent. After optimising the conditions of the extremozyme stage at laboratory scale, the developed extremozyme-aided sequence was validated at pilot scale.

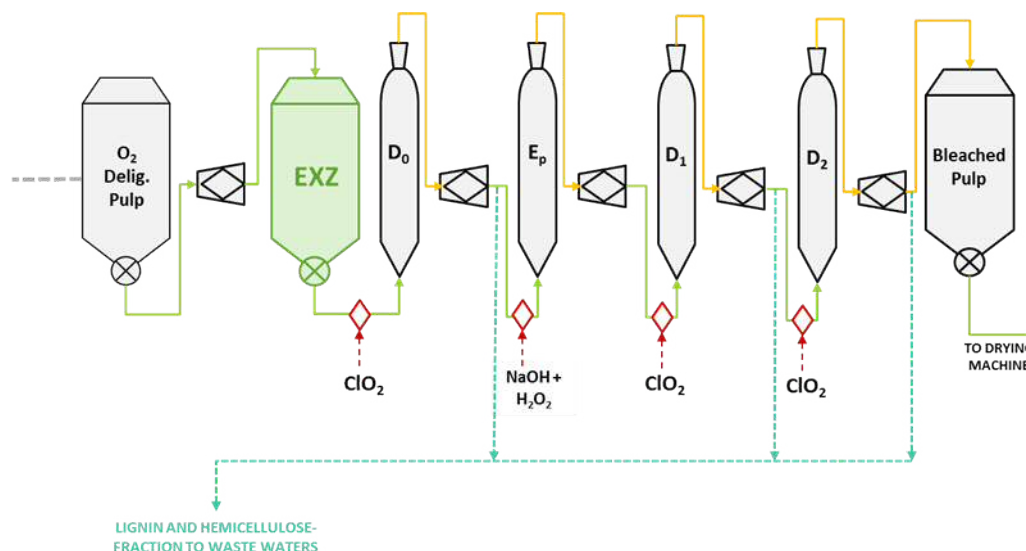
## 2. Results and Discussion

The novel extremophilic xylanase Xyn11 from *Pseudothermotoga thermarum*, with max. activity at pH 10.5 and 90 °C [11], was assayed as a pretreatment stage (EXZ) of industrial oxygen-delignified eucalyptus kraft pulp with the objective of saving  $\text{ClO}_2$ , and compared with the conventional industrial bleaching sequence ( $\text{D}_0\text{E}_p\text{D}_1\text{D}_2$ ) (Figure 1). Three different sets of experiments were carried out to evaluate the effect of introducing an enzymatic stage in the bleaching process and to optimise a xylanase-aided bleaching sequence: EXP (1) optimisation of the duration of the enzymatic stage at the optimal conditions for the activity of the enzyme; EXP (2) reduction in the amount of  $\text{ClO}_2$  required for bleaching the pulp; and EXP (3) evaluation of different extremophilic xylanases.

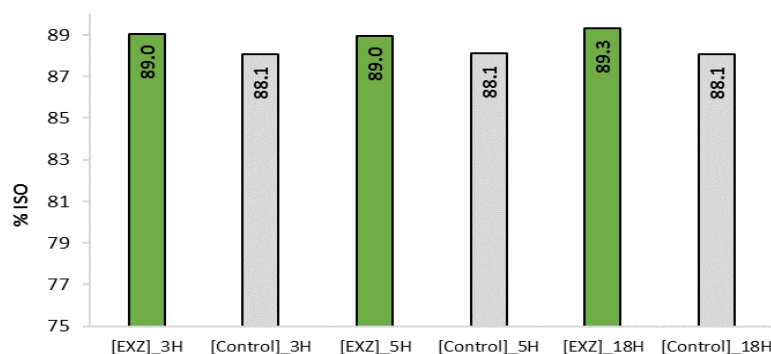
### 2.1. Effect of Xyn11 Pretreatment Duration (EXP 1)

Considering the influence of the reaction time on xylanase effect [7], pulp was treated with Xyn11 during 18 h, 5 h or 3 h. Comparing the final brightness (after  $\text{D}_2$ ) of the resulting pulps, the best result (89.3% ISO) was obtained for the pulp bleached after 18 h of enzymatic treatment (Figure 2). After 3 and 5 h, the final brightness was 0.49 and 0.38% ISO points lower, respectively. The enzymatic prebleaching of the pulp exerted a positive impact on pulp brightness, with gains from 0.77 to 1.25 ISO points, compared to the control pulps,

which showed a final brightness of 88.1% ISO. However, since 18 h of enzymatic treatment is not compatible with mill scale trials, 5 h of reaction was selected to proceed with the next experiments.



**Figure 1.** Scheme of the typical production process of a bleached kraft pulp (grey) with enzymatic treatment, EXZ stage (green), applied after the O<sub>2</sub> delignification stage.

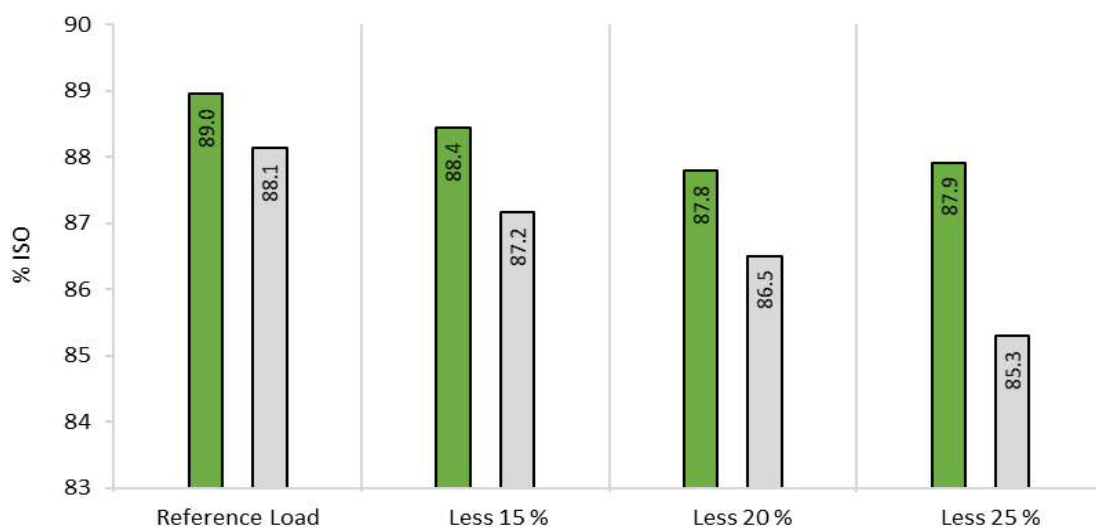


**Figure 2.** Final pulp brightness (after D<sub>2</sub>) obtained through Xyn11 pretreatment for 3, 5 and 18 h, followed by a full bleaching sequence, compared to the corresponding control sequences.

## 2.2. Potential ClO<sub>2</sub> Savings with Xyn11 Pretreatment (EXP 2)

Given the well reported savings of ClO<sub>2</sub>, by applying an enzymatic pretreatment on pulp [5–7,9], three different ClO<sub>2</sub> loads (reduced by 15%, 20% and 25% with respect to the ClO<sub>2</sub> required in the conventional sequence) were assayed. The objective was to confirm the good performance of Xyn11 as bleaching enhancer and to evaluate its potential to reduce the need of the bleaching chemicals, while achieving the industrial reference brightness (88.1% ISO).

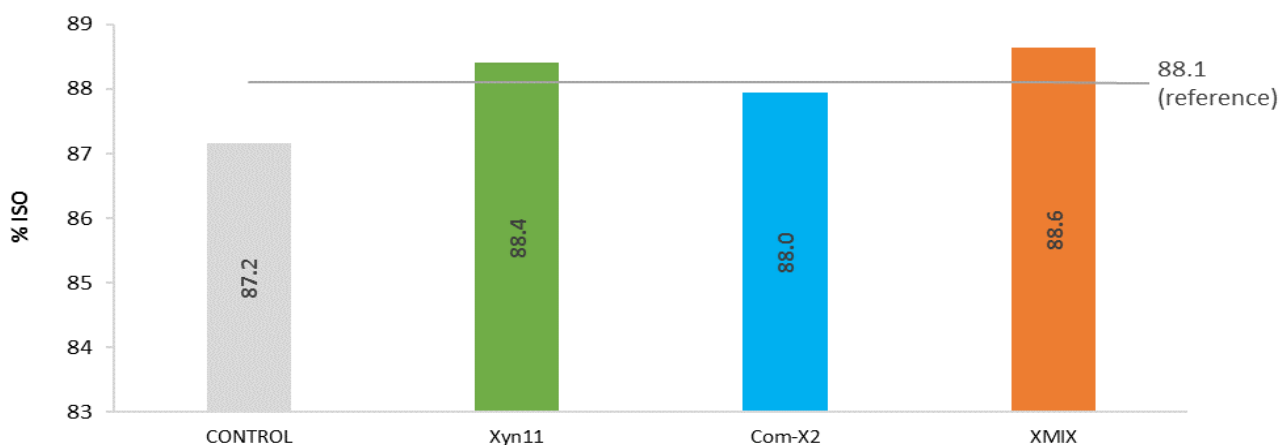
Brightness levels (after D<sub>2</sub>) obtained with the different ClO<sub>2</sub> loads (Figure 3) showed that 15% of ClO<sub>2</sub> can be saved to reach a brightness level of 88.4% ISO, higher than the industrial reference, by adding the 5 h-pretreatment stage with Xyn11. The results obtained for the control pulp with 15% less ClO<sub>2</sub> (87.2% ISO) confirmed the positive effect of the EXZ stage on pulp bleachability.



**Figure 3.** Final pulp brightness (after D<sub>2</sub>) obtained after 5 h prebleaching stage with Xyn11 (green) followed by bleaching with reference ClO<sub>2</sub> load or with 15%, 20% or 25% less ClO<sub>2</sub> in each D step, compared with the corresponding controls (grey).

### 2.3. Comparison between Different Xylanases (EXP3)

Three xylanases, namely Xyn11, a commercial xylanase (Com-X2) and a mix of both (XMIX), were tested as prebleaching stages of the O<sub>2</sub>-delignified eucalyptus kraft pulp using the optimised conditions: 5 h of enzymatic treatment (EXP1) and 15% less ClO<sub>2</sub> in D stages (EXP2). All resulting pulps clearly outperformed the control. Treatments with Xyn11 or XMIX allowed us to achieve a brightness level ( $\geq 88.4\%$  ISO) higher than the industrial reference (Figure 4).

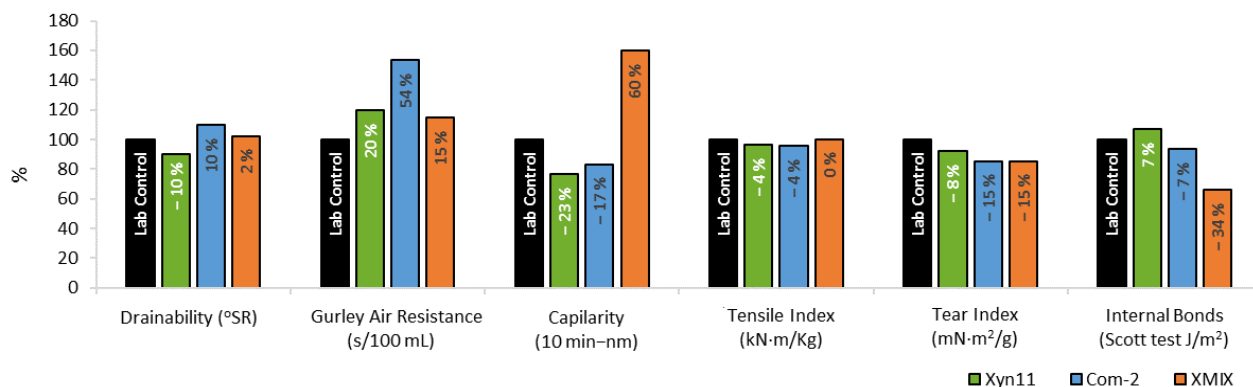


**Figure 4.** Final pulp brightness obtained after 5 h prebleaching stage with different xylanases followed by 15% less ClO<sub>2</sub> applied in each D step of the bleaching sequence.

Papermaking properties were determined to evaluate the effect of the enzymatic stage, and possible differences between the three tested xylanases in terms of the pulp quality. The observed structural properties followed the expected trend; the increase in pulp refining enhanced fibre bonding, leading to a higher drainage index and Gurley air resistance due to the lower amount of water and air (respectively) passing through the fibre network.

Figure 5 shows the papermaking properties of the enzymatically bleached pulps refined with 2000 revolutions (to obtain a drainage index close to the 30 °SR of the market bleached pulp) compared to that of control pulp (with no ClO<sub>2</sub> savings and no enzyme addition). In general, pulp properties were not significantly affected by the enzymatic stages (most variations were within the instrumental error). However, Com-X2 and XMIX

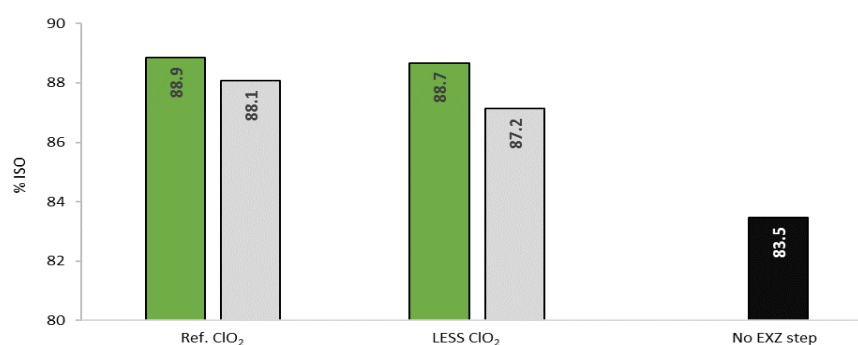
had more impact on the porosity of the fibre network. The internal bonding, tear index and tensile index were less effected by Xyn11 treatment.



**Figure 5.** Papermaking properties obtained for pulps pretreated with different xylanases and bleached with 15% less  $\text{ClO}_2$  compared to the control pulp (no xylanase addition) at laboratory scale.

Despite the reported impact of xylanase in the crystallinity index of cellulose [15], previous work (not published) performed by RAIZ with enzymatic bleaching, led to a reduction in pulp hemicelluloses around 0.5% ( $w/w$ ), indicating that the crystallinity/amorphous ratio of the pulps should not be affected due the low amount of xylyans released. In light of this, the crystalline index of the pulp was determined via X-ray diffraction. No major differences were detected for all the xylanase-treated pulps compared to the control one (Figure S1, Table S1). Thus, it can be inferred that low amounts of xylose were released, as expected.

Taking into account the good pulp brightness level (89.0% ISO) obtained by 3 h treatment with Xyn11 (Figure 2), and given that Xyn11 stage has no detrimental effect on pulp properties, the possibility of saving  $\text{ClO}_2$  with a shorter enzymatic treatment (3 h instead of 5 h) was evaluated. This trial would enable us to define the best performance of EXZ stage combined with the use of bleaching conditions closest to the mill ones before pilot trial validation. Again, 15% less  $\text{ClO}_2$  was added at each D stage of the bleaching sequence ( $\text{D}_0\text{E}_p\text{D}_1\text{D}_2$ ). Three hours of enzymatic treatment were enough to exceed (88.7% ISO) the brightness of the mill reference (88.1% ISO), even when 15% less  $\text{ClO}_2$  was used in the bleaching sequence, confirming the bleaching potential of Xyn11 (Figure 6). The trial also demonstrated the positive effect that the extreme conditions of temperature and pH applied have on pulp brightness, even without the addition of enzyme.



**Figure 6.** Comparison of pulp brightness obtained after 3 h pretreatment with Xyn11 (green) or without enzyme (control, grey) followed by conventional bleaching sequence applying reference or 15% less  $\text{ClO}_2$  loadings; and with 15% less  $\text{ClO}_2$  but without EXZ step (No EXZ step, black).

#### 2.4. Pilot Validation of the Xyn11-Assisted Bleaching of Eucalyptus Kraft Pulp

To validate the laboratory results, the optimised EXZ-assisted bleaching sequence was accomplished at pilot scale on washed  $\text{O}_2$ -delignified pulp under relevant industrial conditions. This pulp had a brightness of 57% ISO, a kappa number of 11 and a drainage

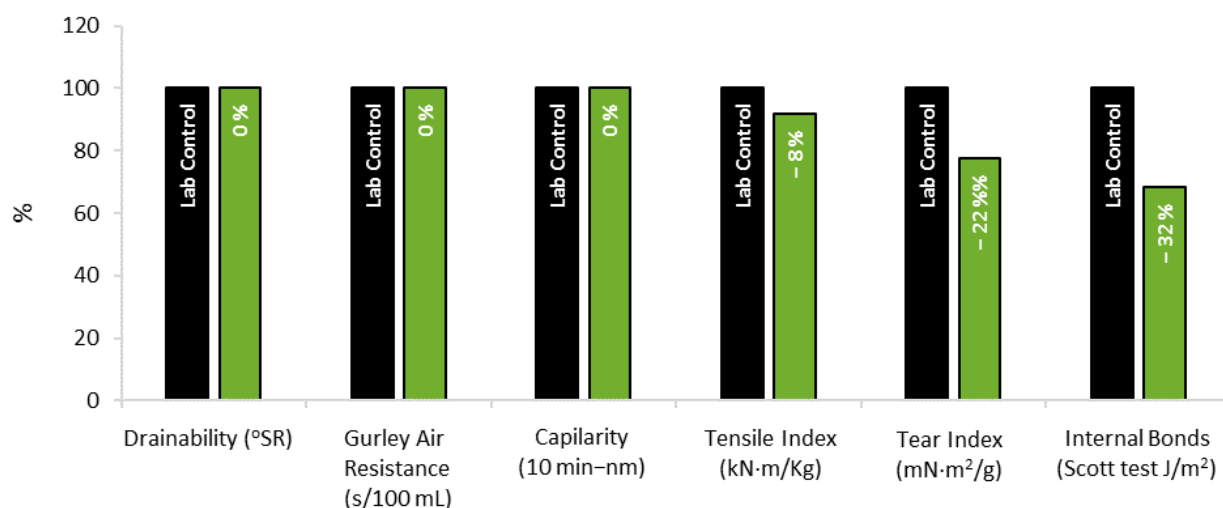
index of 18 °SR. The reference industrial bleaching sequence increased the brightness of the pulp to 89.0% ISO, with 100% ClO<sub>2</sub> used. In contrast, the integration of the EXZ stage in the bleaching sequence allowed us to reach 91.1% ISO brightness after D<sub>2</sub> stage, using 15% less ClO<sub>2</sub> (Table 1), thus confirming it is possible to save ClO<sub>2</sub> and outperform the reference industrial brightness. The brightness of the pulp bleached with the Xyn11-assisted sequence after D<sub>1</sub> stage (90.7% ISO) was already higher than that of the reference mill pulp after D<sub>2</sub>. Therefore, additional ClO<sub>2</sub> savings are achievable. Indeed, it is possible to save 25% of ClO<sub>2</sub> by suppressing the final D<sub>2</sub> bleaching stage in the EXZ-aided bleaching sequence.

**Table 1.** Final properties of the O<sub>2</sub>-Delignified eucalyptus kraft pulp (after D<sub>2</sub> bleaching stage) for the enzymatic sequence (EXZD<sub>0</sub>EpD<sub>1</sub>D<sub>2</sub>) using less 15% ClO<sub>2</sub>, and for the reference sequence (D<sub>0</sub>EpD<sub>1</sub>D<sub>2</sub>) with ClO<sub>2</sub> reference loading.

BLEACHING SEQUENCE	EXZD <sub>0</sub> EpD <sub>1</sub> D <sub>2</sub>	D <sub>0</sub> EpD <sub>1</sub> D <sub>2</sub>
Kappa Number (after Ep)	2.8	3.4
Pulp Brightness (% ISO)	91.1	89.0
Cellulose DPv	1240	1120
Drainage Index (°SR)	23	19
ClO <sub>2</sub> Consumption (%)	91	100

The kappa number of the pulp, measured after the extraction stage (E<sub>p</sub>), decreased with the enzymatic pretreatment, suggesting more lignin was released from the fibres even when 15% less ClO<sub>2</sub> was applied in D<sub>0</sub> stage. After the Xyn11-aided bleaching sequence, the degree of polymerisation of cellulose (DPv) was significantly higher than that of the reference bleached pulp, indicating that the cellulose is less degraded and that the lignin is more easily extracted from the fibre wall during the D stages. Finally, the drainage index slightly increased with the Xyn11-assisted bleaching sequence, indicating that the refining of this pulp should be adapted and will generate some electrical energy savings (Table 1).

Regarding the papermaking properties, similar results were obtained for both enzymatically bleached and reference pulps. The quality of the pulp was not compromised by the enzymatic stage before the bleaching sequence (Figure 7).



**Figure 7.** Papermaking properties obtained for the pulp bleached with the Xyn11-assisted sequence with 15% ClO<sub>2</sub> savings (green) in relation to the control (with no xylanase addition) at pilot scale.

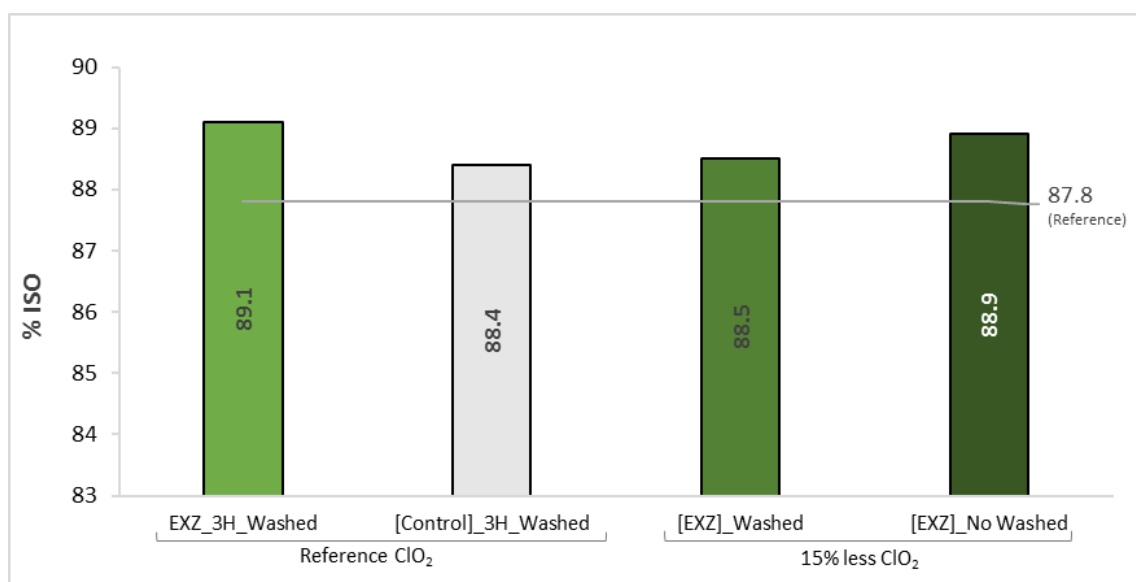
The effluents generated by the EXZ-assisted (EXZD<sub>0</sub>EpD<sub>1</sub>) and reference bleaching (D<sub>0</sub>EpD<sub>1</sub>D<sub>2</sub>) sequences were compared. One important issue in the bleaching of chemical pulps is the generation of organochlorinated compounds. As expected, the EXZ stage did not generate absorbable organic halides (AOX) and, due to the reduction in the ClO<sub>2</sub> charge in each D stage, the total AOX content in the effluent was reduced by 18% at the end of the enzymatic sequence. This 18% global reduction for the whole bleaching effluent

was calculated based on the proportion of each bleaching stage contributing to AOX: 6% reduction for D<sub>0</sub>, 0% for E<sub>p</sub> and 20% for D<sub>1</sub> (Table S2). This reduction in AOX makes the bleaching effluent more amendable to secondary wastewater biotreatments, given AOX are bio-recalcitrant and toxic to anaerobic methanogenic bacteria [15], as well as to aerobic aquatic microorganisms having a negative impact on the biodegradability of the organic matter present in the effluents.

Here, the chemical oxygen demand (COD) of the effluent increased after EXZ stage, most probably due to the higher release of hemicellulose-derived sugars (mainly from xylans) and lignin-based compounds by Xyn11 treatment. However, considering the sum from each bleaching stage, the total COD of the effluent was reduced by 44% after the XD<sub>0</sub>E<sub>p</sub>D<sub>1</sub> sequence (Table S2). The overall biological oxygen demand (BOD) of the effluent from the EXZ-assisted sequence was, however, slightly higher. The higher the BOD/COD ratio, the higher the biodegradability. This indicates that the substances generating the COD are more biodegradable [16]. The EXZ-assisted pulp bleaching generates an effluent which is two times more biodegradable than the control pulp bleaching, reducing the environmental impact and improving the running of the wastewater treatment plant of the mill.

### 2.5. Evaluation of the EXZ-Assisted Bleaching Sequence on Other Hardwood Kraft Pulps

The Xyn11 stage was reproduced on a mixed-hardwoods kraft pulp under the above optimised conditions. The effect of the enzymatic stage was tested on O<sub>2</sub>-delignified pulp with and without washing to evaluate the effect of the residual lignin on the enzyme activity. With the application of the enzymatic treatment before the washing step, it is possible to apply the enzyme directly to the pulp suspension, avoiding the adjustment of the suspension to the optimal pH for the xylanase. Thus, for the trials with less 15% ClO<sub>2</sub>, washed and non-washed pulps were used to evaluate the effect of the original filtrates on Xyn11 performance (Figure 8).



**Figure 8.** Final brightness of a mixed hardwood pulp obtained after bleaching with the EXZ-bleaching sequence. The reference brightness (87.8% ISO) refers to the pulp usually obtained at mill.

Similar results were obtained for mixed-hardwood kraft pulp as for eucalyptus kraft pulp. The introduction of the Xyn11 stage allowed savings of 15% ClO<sub>2</sub> in the bleaching sequence. Both enzymatically treated pulps bleached with 15% less ClO<sub>2</sub> had higher brightness levels than the mill reference (87.8% ISO), suggesting that higher ClO<sub>2</sub> savings may be possible. The best final brightness was obtained with the unwashed pulp (88.9% ISO).

Other studies reported in the literature about pretreatment of hardwood and/or herbaceous kraft pulps with xylanases have proved to reduce the need for chlorine-based chemicals during pulp bleaching. However, some of these reports entail the combined use of xylanase with other enzyme degradation activities to enhance pulp bleachability and achieve comparable chemical savings to those obtained here [8,17–20]. In others, xylanase treatment of kraft pulps does not combine alkaline pH and high temperature [21,22]; these conditions are far from those necessary for a viable integration of the enzymatic step in the industrial process. This is the reason why the potential of xylanases with extremophilic properties as bleaching boosters has been indicated in other studies [23–25].

Moving forward in this line of investigation, it was demonstrated in this work that the feasible extremozyme-assisted ECF bleaching of hardwood kraft pulps at relevant industrial conditions and pilot scale obtained remarkable environmental benefits and bleaching efficiency gains while maintaining pulp brightness and papermaking properties. In addition, the exceptional alkaliphilic properties and thermophilicity of the novel xylanase Xyn11 allows its direct addition to unwashed O<sub>2</sub>-delignified hardwood pulp. This is a significant factor from the industrial point of view, in terms of minimising changes in the current industrial process for pulp production, as the enzymatic stage is carried out at pH 10.5 and 90 °C.

### 3. Materials and Methods

#### 3.1. Raw Material

Industrial O<sub>2</sub>-delignified eucalyptus kraft pulp with 60% ISO brightness and a kappa number around 12 was supplied by a Portuguese mill. This pulp has a brightness close to 60% ISO and a kappa number around 12.

Industrial O<sub>2</sub>-delignified kraft pulp obtained from a mix of hardwoods (poplar, beech, oak and chestnut) was supplied by Fibre Excellence Saint Gaudens mill. This pulp has a 43% ISO brightness and a kappa number of 11. The enzymatic treatment was performed in the O<sub>2</sub>-delignified pulp before and after the washing step. The washing step was carried out on an industrial scale using vapor condensates produced during the cooking process (11 ton of condensates per ton of pulp).

#### 3.2. Enzyme Production

The scale up and pilot scale production of Xyn11 was conducted in 400 L BR300 fermentor (Belach Bioteknik AB, Skogås, Sweden) monitored by Biophantom 2000 (Belach Bioteknik AB, Skogås, Sweden) using MetGen's ENZINE<sup>®</sup> technology platform and *E. coli* production strain [26]. See Table S3 for medium composition. The pH monitoring and control was performed by EasyFerm Plus PHI S8 120 (Hamilton, Bonaduz, Switzerland) automatic addition of 4 M HCl or 28–30% NH<sub>4</sub>OH. Oxygenation of the cells was maintained by constant aeration and automatic increases in stirring. Dissolved oxygen level (set point: 30%) was monitored throughout the cultivation with Hamilton VisiFerm DO ARC 120 (Hamilton). Fermentation was followed by offline monitoring of OD<sub>600</sub>, relative activity and base consumption. Product formation during the fermentation was verified by sampling hourly for xylanase activity determination using endo-1,4-β-D-XYLANASE assay with Azo-Xylan substrate (Birchwood) from Megazyme (Wicklow, Ireland) with the following steps: (1) prepare dilution 1:20 in lysis buffer (1×) using whole cell broth; (2) incubate 20 μL of solution with 130 μL of 0.1 M NaPO<sub>4</sub> Buffer (pH 6.0); (3) incubate samples for 10 min at 45 °C with 1000 rpm; (4) add 150 μL 1% Azo-Xylan solution and continue incubation for 10 min; (5) stop reaction by adding 600 μL 100% EtOH and cool down on ice for 5 min; (6) spin samples and load 200 μL into 96-well plate and measure absorbance at 590 nm.

After fermentation was completed, cells were lysed according to MetGen's standard operation protocols. This includes lysing treatment (18 h, at 25 °C) with lysis solution followed by a heat treatment at 60 °C for 30 min. Lysis solution composition is as follows (per volume or weight for 1 L of lysis solution): Triton X-100—100 mL, Citric acid



anhydrous—34.8 g, NaOH (pH adjustment to 7.0) and DI water for volume adjustment to 1 L. In total, 273 kg of unconcentrated broth was collected and ultrafiltered (Alfa Laval PilotUnit Multi equipped with two Koch Membrane Systems, cut-off 10 kDa). Around 50 kg of product was harvested after ultrafiltration. The product quality was verified by measuring pH profile at 85 °C.

### 3.3. Enzymatic Pretreatment

The enzymatic treatment (EXZ) was applied as a prebleaching stage on O<sub>2</sub>-delignified eucalyptus kraft pulp at the optimum conditions of Xyn11 activity, 90 °C and pH 10.5 [11]. The pulp was previously diluted using mill effluent (from O<sub>2</sub> delignified tower) until it reached a 10% pulp consistency to better reproduce the mill conditions. One ml of Xyn11 was added per 100 g of o.d. pulp at 10% consistency, which represents 5000 units (measured with beechwood xylan at pH 9.0 and 80 °C) per 100 g of pulp.

Next, the pulp was bleached at different stages with a combination of ClO<sub>2</sub>, H<sub>2</sub>O<sub>2</sub> and NaOH, using the conventional bleaching sequence of the mill (D<sub>0</sub>E<sub>p</sub>D<sub>1</sub>D<sub>2</sub>). Total ClO<sub>2</sub> used in D-stages varied between 3.0% and 3.2% o.d. pulp, with a total duration of 325 min at 75 °C. The load of H<sub>2</sub>O<sub>2</sub> and NaOH used on Ep stage varied between 0.44 and 0.66% and 1.22 and 1.77%, respectively. Chemicals loading was adjusted according to the kappa number and brightness of the pulp to process.

### 3.4. Optimisation of the Extremozyme-Bleaching Sequence

Three different sets of experiments were carried out:

EXP 1. The enzymatic treatment was carried out at Xyn11 optimal conditions (90 °C, pH 10.5) during 18 h, 5 h or 3 h at 10% consistency.

EXP 2. This set of experiments were carried out at the best time tested in EXP 1 (5 h) and same conditions, but reducing the amount of ClO<sub>2</sub> by 15%, 20% or 25% in each D stage. The objective was to find the highest savings in ClO<sub>2</sub> that allowed reaching the reference pulp brightness obtained with the control test (88.1% ISO).

EXP 3. In this set of experiments Xyn11, Com-X2 (a commercial MetZyme<sup>®</sup> xylanase provided by MetGen, Kaarina, Finland), and a mixture of both enzymes in a ratio 1:1 *v/v* named XMIX were used in the previously optimised conditions: 5 h, 90 °C and pH 10.5 for EXZ stage, and 15% less ClO<sub>2</sub>.

### 3.5. X-ray Diffraction

Structural analysis of the pulps was performed using the X-ray diffraction technique (XRD, PANalytical, X'Pert Pro model, Almelo, The Netherlands) in a Bragg-Brentano geometry with CuK $\alpha$  radiation ( $\lambda = 1.5406 \text{ \AA}$ ) at 45 KV and 40 mA equipped with X'Celerator detector. The diffractograms were obtained with a range of 0.0501° in an angular amplitude 2 $\theta$  from 10 to 40°. Crystallinity index values were calculated according to the Segal peak height method [27].

### 3.6. Pilot Scale Trial

The Xyn11 stage was conducted at CTP bleaching pilot plant (Grenoble, France) with 110 kg of o.d. pulp, at the conditions optimised at laboratory scale: 1 mL of Xyn11/100 g of o.d. pulp, 90 °C, 3 h, 10% pulp consistency and initial pH of 10.5. The subsequent D<sub>0</sub>E<sub>p</sub>D<sub>1</sub>D<sub>2</sub> sequence was applied with the same conditions as for the reference sequence, except the ClO<sub>2</sub> charge (which is reduced by 15% in each D stage as performed at laboratory scale).

In order to guarantee the chemical integrity and quality of the pulp during the transportation, and considering that the filtrates obtained after oxygen delignification are classified as hazardous substances, which could lead to a considerable delay in the transportation and could compromise the pulp quality, the pilot trial was carried out with washed O<sub>2</sub> delignified eucalyptus kraft pulp, obtained directly from the mill (Portugal). The pulp showed 57% ISO brightness, kappa number of 11 and a drainage index of 18 °SR. About 10 kg of pulp was collected after D<sub>1</sub> in order to compare the pulp quality after the four

stages of the bleaching sequence (EXZ, D<sub>0</sub>, E<sub>p</sub>, D<sub>1</sub>). The pilot trial was stopped at D<sub>1</sub>, since the desired brightness had been reached, but a final D<sub>2</sub> stage was carried out at laboratory scale to see to which level the pulp could be bleached.

The CTP bleaching pilot plant is equipped with a specific reactor, which allows good reproducibility of an industrial bleaching stage, a twin wire press to perform washing and to prepare the pulp for the subsequent bleaching stage, pumps and mixers. At the end of the bleaching sequence, the twin wire press allows pulp sheets to be produced at ≈30% consistency.

### 3.7. Evaluation of Pulp Properties

For all experiments, pulp brightness was measured according to ISO 3688, 1999 and ISO 2470, 2016 standards and compared to the mill reference target. The standard deviation of all brightness measurements varied from 0.1 to 0.3% ISO.

Bleached pulps refined at different refining levels (0, 2000 and 3000 PFI revolutions according to ISO 5264-2 standard) were analysed. The papermaking properties were evaluated according to the standard procedures shown in Table S4. The acceptance of the replicates analysed for each sample are according to the standards presented in Table S4, which consider specific acceptance of error limits in each parameter. The mean values used to build Figures 5 and 7 were computed using only those replicates within the acceptance limits (Table S1). Therefore, all the values presented are accurate according to the demands of the international standards.

### 3.8. Analysis of the Effluents

COD, BOD and AOX content of the bleaching effluents were, respectively, determined according to ISO 15705:2002, NF EN ISO 5815-1 and NF EN 1485 standards.

## 4. Conclusions

A novel bacterial xylanase with outstanding alkaliphilic properties and thermophilicity was successfully overproduced in *E. coli* and used as a prebleaching stage for ECF bleaching of O<sub>2</sub>-delignified hardwood kraft pulps.

The novel Xyn11-assisted bleaching sequence outperformed the bleaching efficiency of the industrial process. A pilot-scale validation of the extremozyme-assisted sequence on eucalyptus kraft pulp under relevant industrial conditions indicated that 25% ClO<sub>2</sub> savings are made possible by removing the last D<sub>2</sub> stage, while maintaining even higher pulp brightness than the mill reference, and with no detrimental effect on the pulp mechanical properties. Moreover, cellulose is less degraded during the D stages and lignin is more selectively extracted. Additional benefits from the reduction of the amount of ClO<sub>2</sub> added in each D stage are the significant decrease in AOX content and a higher biodegradability of the bleaching effluent.

These excellent results were confirmed on a mixed hardwoods kraft pulp, obtaining similar ClO<sub>2</sub> savings, and proving that the enzymatic stage could be directly applied at industrial level without major changes to the current pulp production process.

Finally, for the successful market introduction of a novel methodology or technology for a more sustainable production, technoeconomic performance must be validated. In the case of Xyn11, pilot scale (400 L) production demonstration already indicates a robust process, and the enzyme cost is expected to be at least in line with similar types of enzymes in the market, or even lower. This will enable lower barrier to market for this specific enzyme.

**Supplementary Materials:** The following supporting information can be downloaded at: <https://www.mdpi.com/article/10.3390/ijms232113423/s1>.

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**Conflicts of Interest:** The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

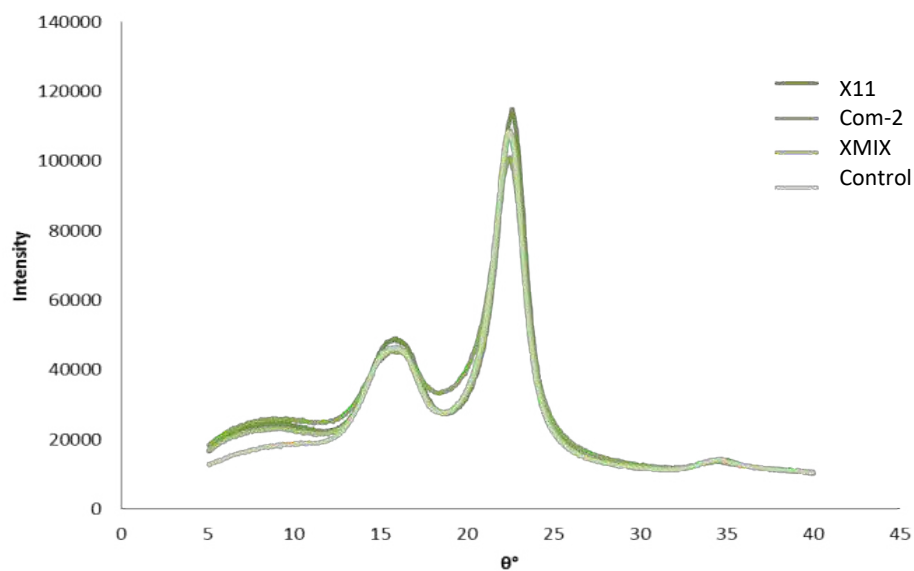
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## Supplementary Material

### Results



**Figure S1.** X-ray diffraction spectra of the pulps treated with the three xylanases (Xyn 11, Com-2, XMIX) compared to the control pulp.

**Table S1.** Crystallinity values for the pulps treated with the three xylanases (Xyn 11, Com-2, XMIX) compared to the control pulp.

Enzyme tested	Crystallinity index of the treated pulp (%)
X11	76.3
Com-2	67.2
XMIX	74.9
Control	74.8

**Table S2.** Analysis of the effluents generated by the Xyn11-assited bleaching (XD<sub>0</sub>E<sub>p</sub>D<sub>1</sub>) of eucalyptus kraft pulp at pilot scale compared with the reference sequence (D<sub>0</sub>E<sub>p</sub>D<sub>1</sub>D<sub>2</sub>).

<b>Bleaching sequence</b>	<b>X D Ep D</b>	<b>D Ep D D</b>
<b>COD, kg/T of o.d. pulp</b>		
After X	8.3	-
After D <sub>0</sub>	5.4	16.0
After Ep	11.9	23.4
After D <sub>1</sub>	1.9	7.6
After D <sub>2</sub>	-	2.6
<b>BOD, kg/T of o.d. pulp</b>		
After X	2.1	
After D <sub>0</sub>	1.6	2.1
After Ep	5.1	5.7
After D <sub>1</sub>	0.9	0.6
After D <sub>2</sub>	-	0.04
<b>AOX, kg/T of o.d. pulp</b>		
After X	0	-
After D <sub>0</sub>	0.15	0.16
After Ep	0.03	0.03
After D <sub>1</sub>	0.04	0.05
After D <sub>2</sub>	-	0.02

## Material and Methods

**Table S3.** Medium composition for production of Xyn 11 at pilot scale in *E. coli*.

Component	g/L
CSL	15
Yeast extract	10
(NH <sub>4</sub> ) <sub>2</sub> SO <sub>4</sub>	0.4
KH <sub>2</sub> PO <sub>4</sub>	2.66
MgSO <sub>4</sub> x 7H <sub>2</sub> O	0.24
K <sub>2</sub> HPO <sub>4</sub>	1.06
Citric acid	0.34
Antifoam	0.2
Technical water	Adjusted for start of fermentation volume

**Table S4.** Standards used for the determination of the papermaking properties.

Papermaking Property	Determination Procedure	Limit for acceptance (%)
Drainage index, Schopper-Riegler	ISO 5267-1:1999	±4%
Air Resistance – Gurley method	ISO 5636-5:2013	±20%
Burst Index	ISO 2758:2015	± 15%
Tensile Index	ISO 1924-2:2008	± 12%
Tear Index	ISO 1974:2012	± 9%
Scott Test	TAPPI 569	± 6%